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## ON THE ROLE OF DISCRETIZATION ERRORS IN THE QUANTIFICATION OF PARAMETER UNCERTAINTIES

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### ABSTRACT

*The independence of numerical and parameter uncertainties is investigated for the flow around the KVLCC2 tanker at  $Re = 4.6 \times 10^6$  using the time-averaged RANS equations supplemented by the  $k - \omega$  two-equation SST model. The uncertain input parameter is the inlet velocity that varies  $\pm 0.25\%$  and  $\pm 0.50\%$  for the determination of sensitivity coefficients using finite-difference approximations. The quantities of interest are the friction and pressure coefficients of the ship and the Cartesian velocity components and turbulence kinetic energy at the propeller plane.*

*A grid refinement study is performed for the nominal conditions to allow the estimation of the discretization error with power series expansions. However, for grids between  $6 \times 10^6$  and  $47.6 \times 10^6$  cells, not all the selected quantities of interest exhibit monotonic convergence. Therefore, the estimates of the sensitivity coefficients of the selected quantities of interest using the local sensitivity method and finite-differences performed for refinement levels that correspond to  $0.764 \times 10^6$ ,  $6 \times 10^6$  and  $47.6 \times 10^6$  cells lead to significantly different values. Nonetheless, for a given grid, negligible differences are obtained for the sensitivity coefficients obtained with two different intervals in the finite-differences approximation.*

*Discrepancies between sensitivity coefficients are compared with the estimated numerical uncertainties. Results obtained in the study suggest that uncertainty quantification performed in*

*coarse grids may be significantly affected by discretization errors.*

### INTRODUCTION

In a study presented in the V&V Symposium of 2019 [1], the independence of numerical and parameter uncertainties was investigated for two-dimensional, incompressible flows over a flat plate and around an airfoil. The simulations were performed with the RANS equations supplemented by eddy-viscosity and transition models and the uncertain input condition was the level of eddy-viscosity at the inlet. In that study, sets of geometrically similar grids were used with a level of grid refinement that allowed reliable estimates of the discretization error (iterative and round-off errors are negligible) using power series expansions. The results suggested that independence of parameter and numerical uncertainties requires attaining smooth convergence with grid refinement, i.e. when the data approaches the so-called asymptotic range.

In the simulation of high Reynolds numbers (turbulent) flows around complex geometries, attaining such level of grid refinement (the asymptotic range) is still rare. On the other hand, uncertainty quantification (UQ) is becoming common practice in engineering applications. However, in many cases it is assumed that the propagation of input uncertainties through a flow solver (one of the most common applications of UQ) is independent

of the discretization error. Therefore, in the interest of saving computational time, uncertainty quantification estimates are often performed with grid refinement levels that lead to significant discretization<sup>1</sup> errors.

This paper repeats the exercise reported in [1] with one main difference: the test case is the flow around the KVLCC2 tanker at  $Re = 4.6 \times 10^6$ , which can be considered a practical test case. In the present exercise, the uncertain input parameter is the inlet velocity that varies  $\pm 0.25\%$  and  $\pm 0.50\%$ . The study is performed with the same options used in [1]: estimates of the sensitivity coefficients of the selected quantities of interest are made using the local sensitivity method and finite-differences [2]; the flow solver is ReFresco [3] that is based on a finite volume discretization of the Reynolds-Averaged continuity and Navier Stokes equations (RANS) supplemented by the two-equation  $k - \omega$  Shear-Stress Transport (SST) eddy-viscosity turbulence model [4].

The flow around the KVLCC2 tanker at model scale Reynolds number has been studied experimentally [5] in a wind tunnel using the so-called double body approach. This means that a symmetric model was used with the symmetry plane located at the still water plane. The main focus of the experimental work was the measurement of the velocity field at six different cross-stream sections at the stern and wake of the ship. For the present exercise, we have selected as quantities of interest the three Cartesian velocity components  $V_x$ ,  $V_y$  and  $V_z$  and the turbulence kinetic energy  $k$  at the 654 locations where experimental data is available. Furthermore, we have also considered the friction  $C_F$  and pressure  $C_P$  resistance coefficients (integral quantities) as quantities of interest.

Flow simulations were performed for a set of 10 nearly geometrical similar multi-block structured grids covering a grid refinement ratio  $r = h_i/h_1$  of approximately 4, where  $h_i$  is the typical cell size of grid  $i$ . Discretization errors of the quantities of interest are estimated with the power law fits presented in [6] using the data of the 6 finest grids that cover a grid refinement ratio of 2. On the other hand, the sensitivity coefficients of the quantities of interest are determined for three grid refinement levels:  $r = 1$ ,  $r = 2$  and  $r = 4$ . Furthermore, the finite-differences approximations are performed with two different intervals of the uncertain input parameter to assess the accuracy of the determination of the sensitivity coefficients for a given grid. These results will allow us to evaluate the influence of the discretization error on the determination the sensitivity coefficients, which is different from evaluating the accuracy of using finite-difference approximations to evaluate sensitivity coefficients for a given grid.

The remainder of this paper is organized in the following way: the test case (governing equations, domain size and boundary conditions) is described in the following section that also contains the definition of the quantities of interest; next, a brief

description of the flow solver is presented including the numerical settings used in the present work; the following section presents the grids sets, the estimation of the numerical errors and the results obtained for the sensitivity coefficients with the three grid refinement ratios selected; the last section presents the main conclusions of this study.

## TEST CASE

### Governing equations

The time-averaged RANS equations for an incompressible fluid are written in strong conservation form as

$$\begin{aligned} \frac{\partial V_i}{\partial x_i} &= 0 \\ \frac{\partial}{\partial x_j} (\rho V_i V_j) &= -\frac{\partial p}{\partial x_i} + \frac{\partial \tau_{i,j}}{\partial x_j}, \end{aligned} \quad (1)$$

where the coordinates of a Cartesian coordinate system  $(x_1, x_2, x_3) \equiv (x, y, z)$ ,  $(V_1, V_2, V_3) \equiv (V_x, V_y, V_z)$  and  $\rho$  is the fluid density. The stress-tensor  $\tau_{i,j}$  is determined using the eddy-viscosity  $\mu_t$  hypothesis that leads to the effective viscosity

$$\mu_{ef} = \mu + \mu_t, \quad (2)$$

with  $\mu$  as the fluid dynamic viscosity.

$$\tau_{i,j} = \mu_{ef} \left( \frac{\partial V_i}{\partial x_j} + \frac{\partial V_j}{\partial x_i} \right). \quad (3)$$

Gravity and part of the normal Reynolds stresses are absorbed in  $p$ , which is defined by

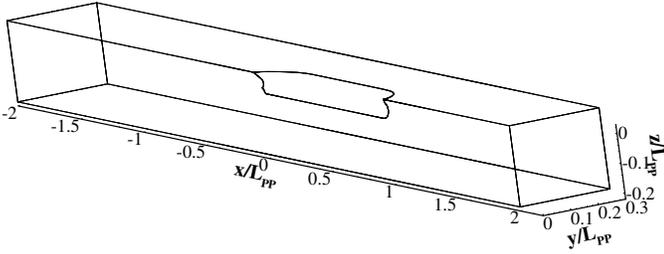
$$p = P - P_h + \frac{2}{3}k, \quad (4)$$

where  $P$  is the average static pressure,  $P_h$  is the hydrostatic pressure and  $k$  is the turbulence kinetic energy. The eddy-viscosity is determined with the two-equation  $k - \omega$  SST model [4] that solves two extra transport equations for  $k$  and the turbulence frequency  $\omega$  to determine

$$\nu_t = \frac{\mu_t}{\rho} = \frac{a_1 k}{\max(a_1 \omega, F_2 S)}. \quad (5)$$

$S$  is the mean strain-rate and the model constants (including  $a_1$ ) and blending functions of the model (including  $F_2$ ) are given in [4].

<sup>1</sup>It should be mentioned that iterative errors may also pollute the numerical solution, but iterative convergence criteria in UQ studies are rarely mentioned.



**FIGURE 1.** Illustration of the computational domain and reference frame used in the calculation of the flow around the KVLCC2 tanker at model scale Reynolds number.

### Geometry and computational domain

The KVLCC2 tanker is a classical test case from the Workshops on CFD in Ship Hydrodynamics [7, 8]. At model scale, the Reynolds number based on undisturbed velocity  $V_\infty$ , distance between perpendiculars  $L_{PP}$  and kinematic viscosity  $\nu$  is  $Re = 4.6 \times 10^6$ . The flow around the KVLCC2 tanker has been extensively studied using RANS and several turbulence models in [9, 10].

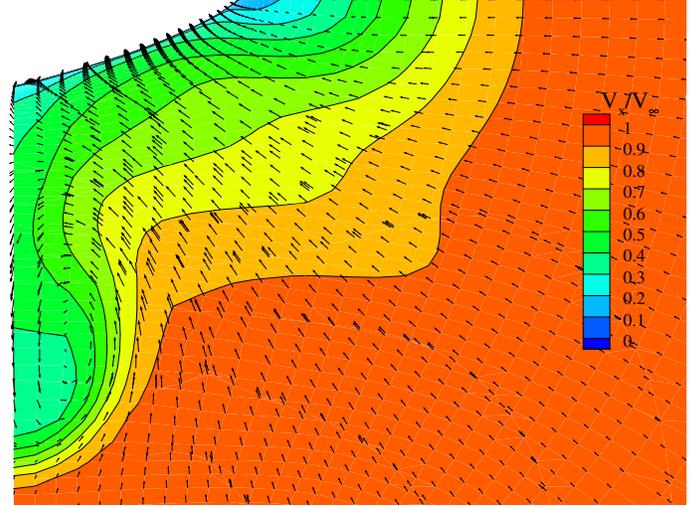
The computational domain is a rectangular prism defined in a Cartesian coordinate system with  $x$  aligned with the incoming flow (pointing to the bow), the transverse  $y$  axis perpendicular to the symmetry plane of the ship ( $y = 0$ ) and the vertical direction  $z$  forming a right-handed system. The origin of the reference frame is located at the intersection of the symmetry plane of the ship, the keel line and the aft perpendicular, as illustrated in Fig. 1.

The cross-section of the computational domain replicates the dimensions of the wind tunnel used by Lee et al. [5]. Due to the two symmetry planes of the tested geometry, only one quarter of the double-body ship is modeled. This leads to a cross-section of  $0.33L_{PP}$  width and  $0.27L_{PP}$  height with the symmetry planes located at  $y = 0$  and  $z = 0.065L_{PP}$  (still water plane). The length of the domain is  $4L_{PP}$  with the inlet boundary placed at  $x = 2L_{PP}$ .

### Boundary conditions

The computational domain includes seven boundaries where boundary conditions must be specified: inlet plane; outlet plane; surface of the ship; symmetry plane of the ship; lateral boundary; bottom boundary and still water plane. Unfortunately, exact boundary conditions are the exception instead of the rule. Nonetheless, we have considered only one uncertain boundary condition which is  $V_x$  at the inlet of the computational domain.

At the inlet boundary,  $V_x = V_\infty$ ,  $V_y = 0$ ,  $V_z = 0$  and the pressure is extrapolated from the interior.  $k$  and  $\omega$  are derived from the reported experimental turbulence intensity  $I = 0.15\%$  [5] and a ratio between turbulent and molecular kinematic viscosities of



**FIGURE 2.** Isolines of the axial velocity component  $V_x$  and transverse velocity field at the propeller plane  $x = 0.0175L_{PP}$  of the flow around the KVLCC2 tanker at model scale Reynolds number.

$\nu_t/\nu = 0.01$ . Sensitivity coefficients of the quantities of interest are determined for intervals of  $\pm 0.25\%$  and  $\pm 0.5\%$  of  $V_x$ .

The pressure is imposed at the outflow boundary and the streamwise derivatives of the remainder dependent variables are set equal to zero. At the lateral ( $y = 0.33L_{PP}$ ) and bottom ( $z = -0.207L_{PP}$ ) boundaries, the normal velocity component is set equal to zero ( $V_z$  for the lateral boundary and  $V_y$  for the bottom boundary) and the derivatives with respect to the normal direction ( $z$  for the lateral boundary and  $y$  for the bottom boundary) of the remainder dependent quantities are set equal to zero.

Velocity components are set equal to zero at the ship surface due to the no-slip and impermeability conditions. The pressure derivative in the direction normal to the ship surface and  $k$  are set equal to zero, whereas  $\omega$  is specified at the nearest wall cell centre [11] using its near-wall analytic solution [12]. The shear-stress at the wall is calculated from its definition, i.e. without wall-functions.

Symmetry conditions are prescribed at the top boundary ( $z = 0.065L_{PP}$ ) and symmetry plane of the ship ( $y = 0$ ).

### Quantities of interest

Two types of flow quantities were selected to check the dependence of the sensitivity coefficients on the discretization error: the friction  $C_F$  and pressure  $C_P$  resistance coefficients obtained from the integration of the shear-stress at the wall and pressure on the ship surface; the Cartesian velocity components  $V_x$ ,  $V_y$  and  $V_z$  and the turbulence kinetic energy  $k$  at the 654 locations of the propeller plane  $x = 0.0175L_{PP}$ , where experimental data is available [5]. The isolines of  $V_x$  and the transverse field

at the propeller plane are illustrated in Fig. 2. The flow exhibits a reduction of  $V_x$  at the centre of the bilge vortex that is essential for the design of the ship propeller.

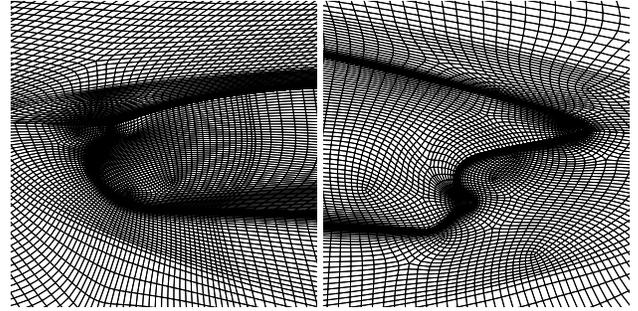
## FLOW SOLVER

ReFRESKO ([www.refresco.org](http://www.refresco.org)) is a community based open-usage CFD code for the Maritime World. It solves multiphase (unsteady) incompressible viscous flows using the Navier-Stokes equations, complemented with turbulence models, cavitation models and volume-fraction transport equations for different phases [13]. The equations are discretized using a finite-volume approach with cell-centered collocated variables, in strong-conservation form, and a pressure-correction equation based on the SIMPLE algorithm is used to ensure mass conservation. The non-linear system of equations<sup>2</sup> for velocity and pressure is linearized with Picards method and either a segregated or coupled approach is used. In the latter, the coupled linear system is solved with a matrix-free Krylov subspace method using a SIMPLE-type preconditioner [14]. A segregated approach is adopted for the solution of all other transport equations. The implementation is face-based, which permits grids with elements consisting of an arbitrary number of faces (hexahedra, tetrahedral, prisms, pyramids, etc.), and if needed h-refinement (hanging nodes). Volume and surface integrals are calculated with second-order mid-point rules and pressure-weighted interpolation [15] is applied for the calculation of the mass fluxes at the faces centre. Several schemes are available for the approximation of the convective and diffusive fluxes (selected schemes are given below). ReFRESKO is currently being developed and verified [16] at MARIN (in the Netherlands), in collaboration with IST (in Portugal) and other non-profit organizations around the world.

## Numerical settings

Second-order schemes were selected for the discretization of the convective and diffusive fluxes of all transport equations, except the  $k$  and  $\omega$  convective fluxes that are approximated with first-order upwind schemes. Non-orthogonality corrections are applied to the diffusive fluxes and eccentricity corrections are used in the determination of gradients at the cells centre using Gauss's theorem.

All calculations are performed in double precision and so the contribution of the round-off error to the numerical error is negligible. Furthermore, iterative convergence requires a maximum value ( $L_\infty$ ) of the normalized residuals below  $10^{-8}$ , which corresponds to mean values of the normalized residuals below approximately  $10^{-10}$ . For each transport equation, residuals are normalized by the main diagonal of the matrix of coefficients and



**FIGURE 3.** Illustration of coarsest grid at the bow and stern regions of the KVLCC2 tanker.

divided by the reference value of the equation dependent variable. Therefore, normalized residuals are equivalent to dimensionless variables changes in a simple Jacobi iteration. These options guarantee that the numerical error is dominated by the discretization error.

## RESULTS

All the results presented in the following sections are dimensionless quantities with  $\rho$ ,  $L_{PP}$  and  $V_\infty$  as the reference quantities. It must be stated that results from simulations performed with different values of  $V_x$  at the inlet ( $\pm 0.25\%$  and  $\pm 0.5\%$ ) also use the nominal value of  $V_\infty$  as the reference velocity.

### Grid sets

A set of 10 nearly-geometrical multi-block structured grids was generated with the GridPro package [17]. The grids range from  $0.764545 \times 10^6$  to  $47.612928 \times 10^6$  cells and the maximum near-wall cell height in wall coordinates  $y_{\max}^+$  varies between 0.6 (coarsest grid) and 0.15 (finest grid). Fig. 3 illustrates the coarsest grid at the bow and stern regions.

The grid refinement ratio  $r_i$  is determined from the total number of cells  $N_{cells}$

$$r_i = \frac{h_i}{h_1} = \left( \frac{N_{cells_1}}{N_{cells_i}} \right)^{\frac{1}{3}}, \quad (6)$$

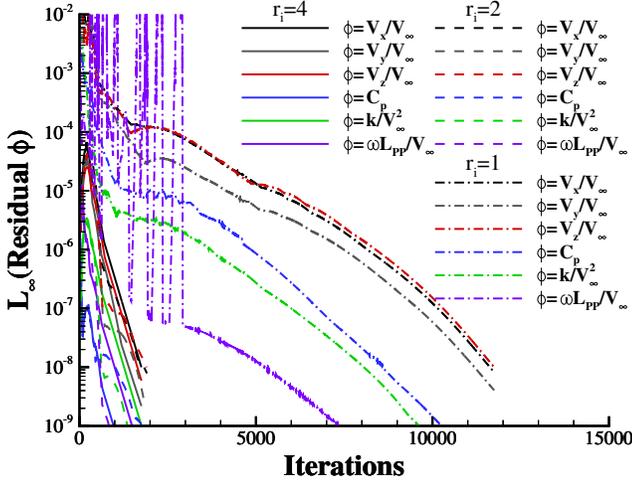
where  $h$  stands for the typical cell size (with 1 denoting the finest grid). In the present grid set,  $1 \leq r_i \leq 4.0$ .

### Reference solution

The estimation of the discretization error of the selected quantities of interest requires an exact solution that is not available. In this study power series expansions [6] are used to obtain a reference (“exact”) solution  $\phi_o$  using

$$\phi_i = \phi_o + \alpha r_i^p. \quad (7)$$

<sup>2</sup>In this paper we only address time-averaged RANS, i.e. statistically steady flow.



**FIGURE 4.** Iterative convergence of the numerical solutions performed in the grids with  $r_i = 4$ ,  $r_i = 2$  and  $r_i = 1$  for the simulation of the flow around the KVLCC2 tanker at model scale Reynolds number.

$\phi_i$  represents a quantity of interest determined in the grid with refinement  $r_i$ ,  $\alpha$  is a constant and  $p$  is the observed order of grid convergence. Eq. (7) is solved in the least-squares sense [6] using the numerical results of the six finest grids that cover a grid refinement ratio of two,  $1 \leq r_i \leq 2$ . As described in [6],  $p$  is limited to values between 0.5 and 2.0. Furthermore, in cases where the least squares solution is unable to determine  $p$  (non monotonic convergence)  $\phi_o$  is estimated from

$$\phi_i = \phi_o + \alpha_1 r_i + \alpha_2 r_i^2, \quad (8)$$

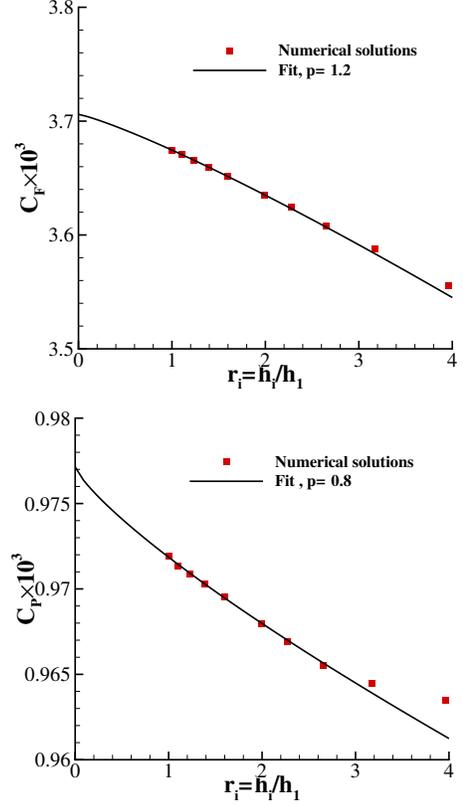
where  $\alpha_1$  and  $\alpha_2$  are constants.

### Iterative convergence

Although iterative errors are reduced to negligible levels in the present study, it is important to illustrate the convergence history of the simulations. Fig. 4 presents the  $L_\infty$  norm of the normalized residuals of all the transport equations for the grid refinement levels  $r_i = 4$ ,  $r_i = 2$  and  $r_i = 1$ . All calculations satisfied the selected iterative convergence criteria. Nonetheless, the iterative convergence rate decreases with the reduction of  $r_i$ , especially for the finest grid ( $r_i = 1$ ). Furthermore, the convergence of  $\omega$  in the finest grid includes several overshoots before exhibiting a smooth convergence.

### Discretization errors

The convergence of the friction  $C_F$  and pressure  $C_P$  resistance coefficients with grid refinement is illustrated in Fig. 5. Both coefficients exhibit monotonic convergence with the observed order of grid convergence slightly larger than one for  $C_F$



**FIGURE 5.** Convergence of the friction  $C_F$  and pressure  $C_P$  resistance coefficients with grid refinement  $r_i$  in the simulation of the flow around the KVLCC2 tanker at model scale Reynolds number.

**TABLE 1.** Estimated discretization errors  $e_{disc}$  of the friction  $C_F$  and pressure  $C_P$  resistance coefficients at three different grid refinement  $r_i$  levels. Flow around the KVLCC2 tanker at model scale Reynolds number.

| $e_{disc}(\%)$ | $r_i = 1$ | $r_i = 2$ | $r_i = 4$ |
|----------------|-----------|-----------|-----------|
| $C_F$          | -0.85     | -1.93     | -4.09     |
| $C_P$          | -0.53     | -0.94     | -1.41     |

and slightly lower than one for  $C_P$ . Table 1 presents the estimates of the discretization errors  $e_{disc}$  of  $C_F$  and  $C_P$  for  $r_i = 1$ ,  $r_i = 2$  and  $r_i = 4$  as a percentage of the values obtained in the finest grid. For these integral quantities, the estimated discretization errors are below 1% for the finest grid ( $r_i = 1$ ), but there is a clear increase of  $e_{disc}$  with grid coarsening, especially for  $C_F$ .

Naturally, we cannot present the convergence with grid refinement of the four local flow quantities ( $V_x$ ,  $V_y$ ,  $V_z$  and  $k$ ) at the 654 locations of the propeller plane ( $x = 0.0175L_{PP}$ ). Therefore,

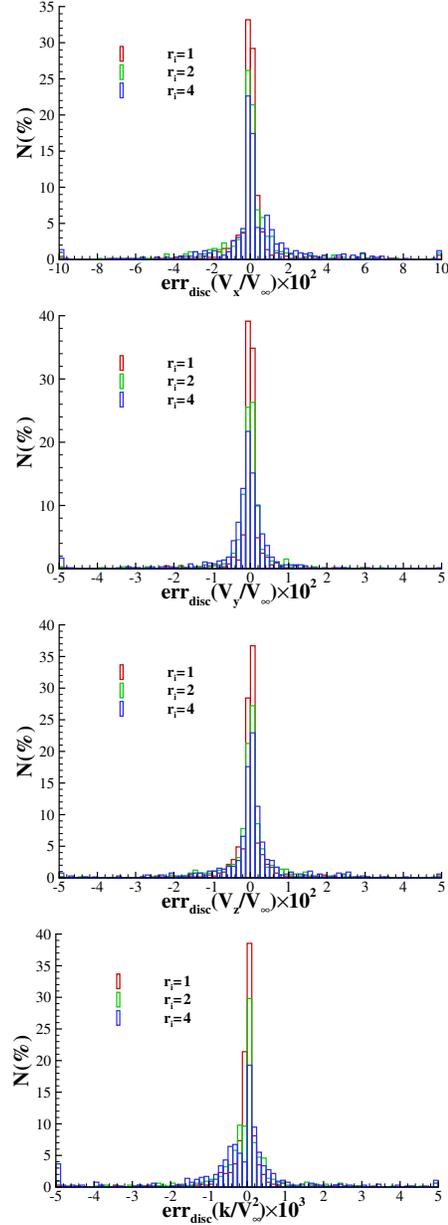
**TABLE 2.** Mean  $\bar{e}_{disc}$  and standard deviation  $\sigma_{e_{disc}}$  of the absolute value of the estimated discretization errors  $|e_{disc}|$  for the Cartesian velocity components ( $V_x/V_\infty$ ,  $V_y/V_\infty$  and  $V_z/V_\infty$ ) and turbulence kinetic energy  $k/V_\infty^2$  at the 654 locations of the propeller plane ( $x = 0.0175L_{PP}$ ). Flow around the KVLCC2 tanker at model scale Reynolds number.

| $r_i$ | $V_x/V_\infty$               |                                 | $V_y/V_\infty$               |                                 |
|-------|------------------------------|---------------------------------|------------------------------|---------------------------------|
|       | $\bar{e}_{disc} \times 10^2$ | $\sigma_{e_{disc}} \times 10^2$ | $\bar{e}_{disc} \times 10^2$ | $\sigma_{e_{disc}} \times 10^2$ |
| 1     | 0.61                         | 1.59                            | 0.19                         | 0.49                            |
| 2     | 1.02                         | 1.94                            | 0.30                         | 0.60                            |
| 4     | 1.49                         | 2.57                            | 0.47                         | 0.97                            |
| $r_i$ | $V_z/V_\infty$               |                                 | $k/V_\infty^2$               |                                 |
|       | $\bar{e}_{disc} \times 10^2$ | $\sigma_{e_{disc}} \times 10^2$ | $\bar{e}_{disc} \times 10^3$ | $\sigma_{e_{disc}} \times 10^3$ |
| 1     | 0.23                         | 0.50                            | 0.31                         | 1.01                            |
| 2     | 0.39                         | 0.65                            | 0.58                         | 1.33                            |
| 4     | 0.60                         | 1.18                            | 1.00                         | 1.86                            |

we characterize the discretization errors of these variables with the histograms of the signed estimated value of  $e_{disc}$  in Fig. (6) and the mean and standard deviations of the absolute value of  $|e_{disc}|$  presented in Table 2.

The results exhibit a similar behaviour for the four variables with almost an equivalent number of locations exhibiting positive or negative errors. There is a systematic increase of  $\bar{e}_{disc}$  and  $\sigma_{e_{disc}}$  with the increase of  $r_i$ , but the mean values of the estimated discretization errors do not double when the refinement ratio is multiplied by 2, which would be roughly the expected behaviour for first order convergence. However, estimating the observed order of grid convergence  $p$  for the present level of grid refinement (six grids between  $6 \times 10^6$  and  $47.6 \times 10^6$  cells) is not trivial. Four different alternatives are used to obtain the data included in Fig. 6 and Table 2 [6]:  $p$  obtained from the data;  $p = 1$ ;  $p = 2$  and 2 terms as defined in Eqn. (8). Table 3 presents the percentage of locations determined with each of these alternatives.

The data presented in Table 3 confirms the difficulties to estimate  $p$  for local quantities of complex turbulent flows calculated with the RANS equations. Surprisingly,  $k$  is the variable that exhibits more locations where  $p$  is determined from the data, but it is still less than 30% of the locations. Nonetheless, the average value of  $p$  estimated from the data is close to 1.3 for the four flow variables. On the other hand, the results also indicate that are still roughly 10% of the locations where the solutions are not converging monotonically for grids with more than  $6 \times 10^6$  cells, which presents again a challenge for the estimation of discretiza-



**FIGURE 6.** Histograms of the signed estimated value of  $e_{disc}$  for the Cartesian velocity components ( $V_x$ ,  $V_y$  and  $V_z$ ) and turbulence kinetic energy  $k$  at the 654 locations of the propeller plane ( $x = 0.0175L_{PP}$ ). Flow around the KVLCC2 tanker at model scale Reynolds number.

tion errors.

### Sensitivity coefficients

As for the study reported in [1], the main goal of this study is to address the influence of numerical (discretization) errors on the estimation of the sensitivity coefficients of the quantities of

**TABLE 3.** Percentage of cases for the four alternatives used in the estimation of the discretization errors  $e_{disc}$ . Cartesian velocity components ( $V_x/V_\infty$ ,  $V_y/V_\infty$  and  $V_z/V_\infty$ ) and turbulence kinetic energy  $k/V_\infty^2$  at the 654 locations of the propeller plane ( $x = 0.0175L_{PP}$ ). Flow around the KVLCC2 tanker at model scale Reynolds number.

| Variable | Eqn. (7) |         |         | Eqn. (8) |
|----------|----------|---------|---------|----------|
|          | $p$ data | $p = 1$ | $p = 2$ | 2 terms  |
| $V_x$    | 15.7     | 30.4    | 44.8    | 9.1      |
| $V_y$    | 18.5     | 25.7    | 45.0    | 10.8     |
| $V_z$    | 16.4     | 27.7    | 46.0    | 9.9      |
| $k$      | 29.7     | 14.5    | 43.3    | 12.5     |

**TABLE 4.** Sensitivity coefficients of the friction  $C_F$  and pressure  $C_P$  resistance coefficients obtained for three levels of grid refinement  $r_i$ .  $\Delta$  stands for  $((V_\infty)_p - (V_\infty)_m) / V_\infty$ ,  $C_{F_0}$  and  $C_{P_0}$  stand for the values obtained in the finest grid  $r_i = 1$  using the nominal value of  $V_\infty$ . Flow around the KVLCC2 tanker at model scale Reynolds number.

| $r_i$ | $S(C_F)_{V_\infty} \times V_\infty / C_{F_0}$ |                 | $S(C_P)_{V_\infty} \times V_\infty / C_{P_0}$ |                 |
|-------|---|-----------------|---|-----------------|
|       | $\Delta = 0.005$                              | $\Delta = 0.01$ | $\Delta = 0.005$                              | $\Delta = 0.01$ |
| 1     | 1.839   | 1.839           | 1.786   | 1.786           |
| 2     | 1.813   | 1.813           | 1.771   | 1.771           |
| 4     | 1.763   | 1.763           | 1.754   | 1.755           |

interest using central-differences that lead to

$$S(\phi)_{V_\infty} = \frac{\partial \phi}{\partial V_\infty} \simeq \frac{\phi_p - \phi_m}{(V_\infty)_p - (V_\infty)_m}, \quad (9)$$

where  $\phi$  stands for the quantity of interest and the subscripts  $p$  and  $m$  identify the two extra simulations performed to obtain the sensitivity coefficient. In this case we have used  $((V_\infty)_p - (V_\infty)_m) = 0.01V_\infty$  and  $((V_\infty)_p - (V_\infty)_m) = 0.005V_\infty$  to apply Eqn. (9) for all selected quantities of interest using three grid refinement levels:  $r_i = 1$ ,  $r_i = 2$  and  $r_i = 4$ . All sensitivity coefficients are presented in dimensionless form, which means that  $S(\phi)_{V_\infty}$  is multiplied by  $V_\infty$  and divided by  $\phi_0$  that corresponds to the quantity of interest obtained in the finest grid ( $r_i = 1$ ) using the nominal value of  $V_\infty$ .

Table 4 presents the sensitivity coefficients obtained for the resistance coefficients  $C_F$  and  $C_P$  using the two different intervals of  $((V_\infty)_p - (V_\infty)_m)$ . The sensitivity coefficients obtained from the two intervals are (almost) identical and indicate that

**TABLE 5.** Number of cases with an absolute percentual change of  $S(\phi)_{V_\infty}$  obtained with  $r_i = 2$  or  $r_i = 4$  when compared to  $S(\phi)_{V_\infty}$  determined with  $r_i = 1$  larger than 5%. Results for the Cartesian velocity components ( $V_x$ ,  $V_y$  and  $V_z$ ) and turbulence kinetic energy  $k$  at the 363 locations of the propeller plane ( $x = 0.0175L_{PP}$ ) that exhibit  $V_x \leq 0.9V_\infty$ . Flow around the KVLCC2 tanker at model scale Reynolds number.

| $r_i$ | $V_x$ | $V_y$ | $V_z$ | $k$  |
|-------|-------|-------|-------|------|
| 2     | 9.85  | 25.1  | 29.8  | 54.7 |
| 4     | 24.1  | 36.7  | 49.7  | 88.7 |

a change of 1% in the value of  $V_\infty$  produces a change of the resistance coefficients of approximately 1.8%. On the other hand, the influence of the grid refinement level on  $S(C_F)$  is larger than on  $S(C_P)$  with the main differences obtained between the  $r_i = 1$  and  $r_i = 4$  solutions, as expected. However, the largest differences between dimensionless sensitivity coefficients are smaller than 0.07, which is not a completely unexpected result considering that the convergence of the two variables illustrated in Fig. 5 is smooth and monotonic.

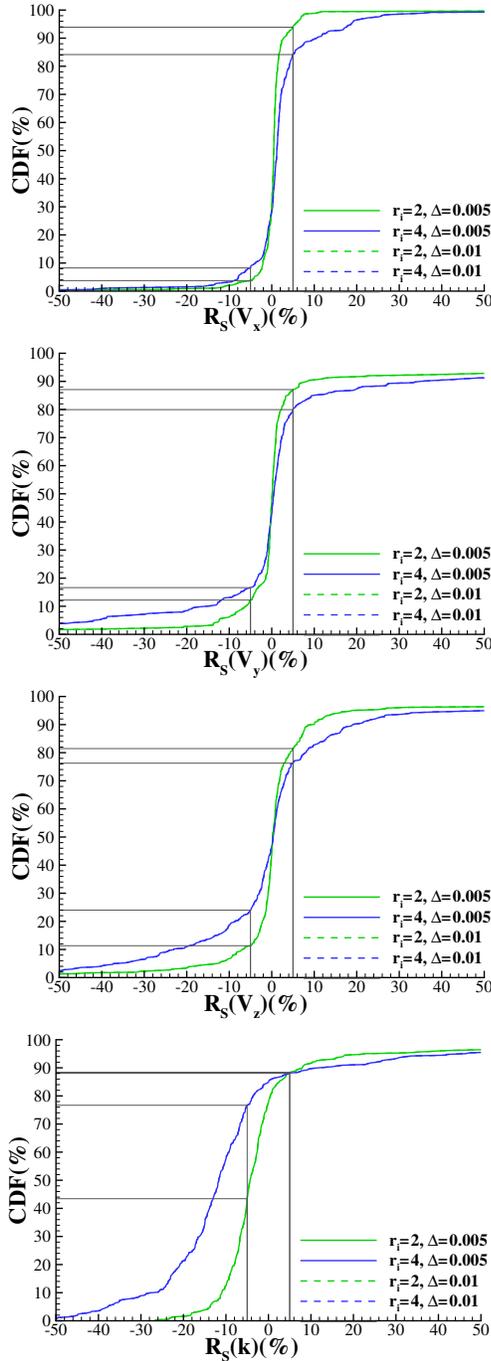
Addressing the effect of discretization errors on the estimation of the sensitivity coefficients of the local quantities of interest is more troublesome. There are four variables ( $V_x$ ,  $V_y$ ,  $V_z$  and  $k$ ) at 654 locations and so the data must be handled statistically. The percentual change of  $S(\phi)_{V_\infty}$  obtained with  $r_i = 2$  or  $r_i = 4$  when compared to  $S(\phi)_{V_\infty}$  determined with  $r_i = 1$  is calculated from

$$R_S(\phi) = \left( \frac{S(\phi)_{V_\infty}(r_i)}{S(\phi)_{V_\infty}(r_1)} - 1 \right) \times 100. \quad (10)$$

$R_S(\phi)$  is determined only at the 363 locations that exhibit  $V_x \leq 0.9V_\infty$  to avoid the region where viscous effects are negligible. The results are presented in Fig. 7 that includes the cumulative density functions (CDFs) of  $R_S(V_x)$ ,  $R_S(V_y)$ ,  $R_S(V_z)$  and  $R_S(k)$ .

The results obtained with the two intervals of  $V_\infty$  tested are graphically identical. The variable that shows the smallest influence of the discretization error on the estimation of the sensitivity coefficients is  $V_x$ , whereas  $S(k)_{V_\infty}$  exhibits the largest changes with  $r_i$ . The CDFs of  $R_S(\phi)$  are not symmetric (that would mean CDF=50% for  $R_S(\phi) = 0$ ) and the shape of the CDF depends on the selected flow variable and level of grid refinement. Nonetheless, it is clear that for the present levels of grid refinement tested the sensitivity coefficients are dependent on the numerical (discretization) error.

Table 5 presents the percentage of cases that exhibits  $|R_S(\phi)|$  larger than 5%. It is clear that the effect of the numerical (discretization) error on the determination of  $S(\phi)_{V_\infty}$  is not negli-



**FIGURE 7.** Cumulative density functions of the percentual change of  $S(\phi)_{V_\infty}$  obtained with  $r_i = 2$  or  $r_i = 4$  when compared to  $S(\phi)_{V_\infty}$  determined with  $r_i = 1$ . Results for the Cartesian velocity components ( $V_x$ ,  $V_y$  and  $V_z$ ) and turbulence kinetic energy  $k$  at the 363 locations of the propeller plane ( $x = 0.0175L_{PP}$  that exhibit  $V_x \leq 0.9V_\infty$ ). Flow around the KVLCC2 tanker at model scale Reynolds number.

ble. The estimation of the  $k$  sensitivity coefficients on the coarsest grid ( $r_i = 4$ ) may be completely misleading and the same observation also applies to the  $V_y$  and  $V_z$  velocity components.

## CONCLUSIONS

This paper presents a study about the dependence of the estimation of sensitivity coefficients on the numerical (discretization) error, which assesses the independence of numerical and input uncertainties. The test case is the flow around the KVLCC2 tanker at model scale Reynolds number and the quantities of interest include integral parameters (resistance coefficients) and local variables (Cartesian velocity components and turbulence kinetic energy) at the propeller plane.

Grid refinement studies were performed with grids ranging from  $0.76 \times 10^6$  and  $47.6 \times 10^6$  cells using the time-averaged RANS equations supplemented by the  $k - \omega$  SST two-equation eddy-viscosity turbulence model. Sensitivity coefficients are evaluated for three levels of grid refinement:  $r_i = 1$  (finest grid);  $r_i = 2$  and  $r_i = 4$  (coarsest grid).

The results suggest the following conclusions:

The grid refinement level to obtain negligible discretization errors in RANS solutions of complex turbulent flows is most likely much more demanding than the typical values published in the open literature.

For “practical applications” including turbulent flows, the determination of sensitivity coefficients in coarse grids may lead to results significantly polluted by discretization errors.

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